



Remediation of Aqueous Solution of Cypermethrin and Chlorpyrifos Using Derived Adsorbent from *Jatropha Curcas*

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ABSTRACT: The study focused on assessment of removal of cypermethrin and chlorpyrifos in aqueous solution using activated carbon made from *Jatropha Curcas*. Batch adsorption experiments were carried out under different conditions of parameters such as pH, contact time, adsorbent dosage, and initial concentration of the adsorbate on pesticide adsorption. The adsorption data were described by Langmuir and Freundlich adsorption model. Adsorption capacity of 92.73% and 92.26% of chlorpyrifos and cypermethrin respectively were removed by 2g of the adsorbent per 50 cm³ of initial concentration of 0.78 mg/l and 1.50 mg/l chlorpyrifos and cypermethrin respectively. This was achieved at 90 min of the contact time and at optimum pH of 6.3. The study demonstrates that the activated carbon made from *Jatropha Curcas* can be effective in the adsorption of these two pesticides from water bodies. Equilibrium experiment results show that adsorption isotherms of cypermethrin and fit better to Freundlich adsorption isotherm while chlorpyrifos fit better on the Langmuir adsorption isotherm

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Safety in our environment has been the focus of the day. A major factors constituting to enormous threat to environment is pesticides pollution. Pesticides are artificially synthesized, toxic bio accumulative agents. Chemical pesticides are frequently applied in agricultural activities to ensure good harvest (Chang *et al.*, 2011) The ongoing and uncontrolled use of pesticide to fight pest and improve agricultural production constitutes a risk for water quality (Mirjana *et al.*, 2010). The pesticides have been detected by monitoring surface and underground waters. According to European Union Directives and Regulations for drinking water hygiene, the maximum allowed concentration of total pesticides is 0.5µg dm⁻³ (Mirjana *et al.*, 2010). The problem of chemical pesticides in the environment is a social issue as the contaminant were frequently detected in the different water sources, rivers and soil. The leaching runs off from agricultural forest land & even residential places. The toxicity of pesticide and their degradation products is making these chemical substances a potential hazard (Salman *et al.* 2010).

Chlorpyrifos (O,O-diethyl O-3,5,6-trichloro-2-pyridyl phosphorothioate) is a common organophosphorus insecticide, widely used active ingredient for the protection of important agricultural crops such as corn, citrus, peanuts, etc and also effective in controlling a variety of insects including

worms, cockroaches, flies, termites, fire ant and lice. On the other hand Cypermethrin is a pyrethroid pesticide and is used in the control of a wide range of insects on crops like vegetables, cereals and maize (USEPA, 2002). Conventional waste water technologies for treating pesticides wastewater and industrial effluents include chemicals, biological and physical treatments such as coagulation and flocculation, ozonation, electrochemical processes, nano filtration, and adsorption (Okeola *et al.*, 2014; The following conventional methods were used for removal of some pesticides in wastewaters Fenton with coagulation (Chen *et al.*, 2007), photo catalysis and electro-Fenton, combined ultrasound and Fenton (Ma *et al.*, 2010), Oxidants and photolysis, biological degradation (Singh *et al.*, 2008) and adsorption (Ignatowicz, 2009). However, adsorption process is one of the most widely applied techniques for pollutant removal. Adsorption plays a significant role in the environmental pollution control. The common adsorbents include activated carbon molecular sieves polymeric adsorbents and some other low cost material. Among numerous clean-up techniques, adsorption technique with activated carbon from agricultural material or waste is ecofriendly. Such sources include bamboo, coconut shell, chestnut shells (Memon *et al.*, 2007) and snail shell (Udeozor and Ebuomwan 2014). Adsorbents derived from *jatropha curcas* has been used effectively for various

adsorptions, Raw treatment *jatropha curcas* was applied for adsorption of aqueous Cu (II) ion adsorption (Jain *et al* 2008), activated carbon processed from the shell of this crop has been used for adsorption of methylene blue (Okeola *et al* 2010), adsorption of Congo red (Okeola *et al* 2014), Removal of Fe (II) ion (Okeola and Odebunmi 2011).

Therefore this work is to determine the feasibility of application of the activated carbon from *jatropha curcas* shell for the adsorption of the pesticides cypermethrin and Chloropyrifos Thus reducing or removing them from aqueous environment.

MATERIALS AND METHODS

Adsorbate and adsorbent: The adsorbent employed is the already produced activated carbon from *jatropha curcas* shell. This has been used for effective adsorption of methylene blue and acetic acid (organic solutes) and potassium permanganate (inorganic solute).Chloropyrifos and cypermethrin were procured from an agrochemical plaza along Ilorin,Kwara state, Nigeria. A 100mg/L solution of Cypermethrin pesticide was prepared by taking 1ml of the stock solution 100 g/L into 1000ml standard flask. Subsequent solutions of lower concentration were made by serial dilution.

Batch equilibrium studies: Batch adsorption experiments were carried out using a series of erlenmeyer flasks. The experiments were conducted to investigate the effect of pH contact time,initial pesticide concentration and adsorbent dosage. All the adsorption experiments were carried out at room temperature (30 ± 2°C). The initial pH was adjusted with 0.1M HCl or 0.1M NaOH. Time course experiments were investigated by shaking the sorption mixture of (adsorbent and adsorbate) at various predetermined interval and conditions. The mixtures left were filtered and the filtrate analysed for the adsorbate concentration, blank solutions without adsorbent were also shaken and the concentrations determined. This was used as initial concentration. The concentrations of pesticide in the solution before and after adsorption were determined using a double beam UV-Vis spectrophotometer (Shimadzu DU 730) at its maximum wavelength of 300 nm and 375 nm for Chloropyrifos and cypermethrin respectively. Each batch of the experiment were duplicated under identical conditions and the results obtained from their means. In the determination of adsorption capacity of solute intake per unit mass of activated carbon (q_e, mg/g) was calculated using adsorption system mass balance as shown in equation (i)

$$q_e = \frac{V (C_i - C_f)}{w} \dots\dots\dots (i),$$

Where v = volume of solution (L)
 w = amount of dry adsorbent/ substrate (g)
 c_i = initial concentration (mg/l) and
 c_f = final concentration (g)

The percentage of dye uptake (% uptake) was also calculated in some cases using the equation (ii);

$$\% \text{ uptake} = \frac{c_i - c_f}{c_i} \times 100 \dots\dots\dots (ii)$$

Determination of Effect of adsorbent dosage on chlorpyrifos and cypermethrin: The effect of adsorbent dosage on adsorption of chlorpyrifos and cypermethrin was studied using initial concentration of 0.78 mg/l and 1.50mg/l respectively for different amount of the adsorbent (0.1, 0.2, 0.5, 1.0, 1.5, 2.0, 3.0) g that were separately weighed into different sample bottles. A 50ml of the same concentration of each of the pesticide solution was added into each sample bottles containing the adsorbent.

was shaken on mechanical shaker at various time intervals between 15-105 mins. The clear solution was analysed for the residual pesticide concentration.

Determination of Effect of pH on chlorpyrifos and cypermethrin: The pH of the solution is an important controlling parameter in the adsorption process. The effect of pH on the equilibrium sorption of each pesticide was investigated by employing an initial concentration of chlorpyrifos and cypermethrin, 0.78 mg/l and 1.50 mg/l respectively and 0.2 g of activated carbon (TSC) in 50 ml of solution. The suspensions were shaken for 100 min and the amount of pesticide adsorbed determined. The experiment was repeated for pH 2.2-7.5.

Determination of Effect of initial concentration on chlorpyrifos and cypermethrin: The effect of initial concentration of chlorpyrifos and cypermethrin

concentration on adsorption was investigated. The experiments were carried out at a fixed dose of activated carbon (0.2 g), temperature 30°C, pH 6.3 and different initial concentration of pesticide, range of 1.5 – 1.8 mg/l.

Evaluation of Adsorption Isotherm of chlorpyrifos and cypermethrin: The capacity of the adsorption isotherm is fundamental, and plays an important role in the determination of the maximum capacity of adsorption. It also provides a panorama of the course taken by the system under study in a concise form, indicating how efficiently an adsorbent will adsorb and allows an estimate of the economic viability of the adsorbent commercial applications for the specific solute. In order to adapt for the considered system, an adequate model that can produce the experimental results obtained, equations of Langmuir and Freundlich, have been considered. The two models

have been the most widely used isotherm equation. Construction of Adsorption Isotherm was carried out from the batch adsorption experiment of effect of initial concentration by adding 0.2 g fixed dose of activated carbon temperature 30°C, pH 6.3 and different initial concentration of pesticide, range of 1.5 – 1.8 mg/l.

Freundlich Adsorption Isotherm: The Freundlich isotherm model is an empirical relationship describing the adsorption of solutes from a liquid to a solid surface assumes that different sites with several adsorption energies are involved. Freundlich adsorption isotherm is the relationship between the amounts of solute adsorbed per unit mass of adsorbent, q_e , and the concentration of the solute at equilibrium, C_e . This isotherm can be described as in equation (iii)

$$\log q_e = \log K_f + \frac{1}{n} \log C_e \dots\dots\dots (iii)$$

Where q_e (mg/g) is the adsorption capacity at equilibrium, C_e (mg/L) is the equilibrium concentration of adsorbate in solution and K_f (mg/g) and n are the Freundlich physical constants, both are the indicator of the adsorption capacity and adsorption intensity respectively. (Ma et al 2010).

Langmuir Adsorption Isotherm: The Langmuir model is based on the assumption that the maximum adsorption occurs when a saturated monolayer of solute molecules is present on the adsorbent surface, the energy of adsorption is constant and there is no migration of adsorbate molecules in the surface plane. (Kumar and Gayathri 2009 ; Okeola and Odebunmi ,2010) The Langmuir isotherm is given in equation (iv)

$$\frac{1}{q_e} = \frac{1}{q_m} + \frac{1}{q_m KL C_e} \dots\dots\dots (iv)$$

Where q_m (mg/g) and KL (L/g) are the Langmuir constants representing the maximum monolayer adsorption capacity for the solid phase loading and the energy constant related to the heat of adsorption respectively.

RESULTS AND DISCUSSION

Effect of adsorbent dosage on adsorption of pesticides: In the studies the adsorption percent (%) of the respective pesticides was found to vary with different mass samples. From data presented in Table1, it shows that the suitable mass of activated carbon is (2g). The adsorption percent 92.73% and

92.26% for chlorpyrifos and cypermethrin respectively was observed. A similar result was observed for the removal of carbofuran and chlorpyrifos from aqueous solution using walnut shells (Memon et al 2007)

Table 1 Percentage adsorption of cypermethrin and chlorpyrifos at different mass of adsorbent

| Adsorbate | Mass of adsorbent (g) | Co (mg/l) | Ce (mg/l) | X(mg/l) | % Adsorption |
|--------------|-----------------------|-----------|-----------|---------|--------------|
| Cypermethrin | 0.1 | 1.5 | 1.129 | 0.371 | 24.74 |
| | 0.2 | 1.5 | 0.728 | 0.772 | 51.46 |
| | 0.5 | 1.5 | 0.574 | 0.926 | 61.75 |
| | 1.0 | 1.5 | 0.437 | 1.063 | 70.86 |
| | 1.5 | 1.5 | 0.257 | 1.243 | 82.86 |
| | 2.0 | 1.5 | 0.116 | 1.384 | 92.26 |
| Chlorpyrifos | 3.0 | 1.5 | 0.116 | 1.384 | 92.26 |
| | 0.1 | 0.78 | 0.672 | 0.108 | 15.11 |
| | 0.2 | 0.78 | 0.651 | 0.129 | 52.31 |
| | 0.5 | 0.78 | 0.544 | 0.236 | 55.75 |
| | 1.0 | 0.78 | 0.145 | 0.635 | 71.97 |
| | 1.5 | 0.78 | 0.061 | 0.719 | 89.78 |
| | 2.0 | 0.78 | 0.057 | 0.723 | 92.73 |
| | 3.0 | 0.78 | 0.057 | 0.723 | 92.73 |

pH = 6.3, time 1.5hr temp. 30°C

Effect of contact time on adsorption of chlorpyrifos and cypermethrin: The influence of contact time on adsorption capacity of chlorpyrifos and cypermethrin is shown in table 2. The results clearly show that the adsorption of chlorpyrifos and cypermethrin increases with time until reaching a nearly saturation level. Rate of uptake of each pesticide is higher at the beginning which may be due availability of a large number of active sites on the adsorbent. As the sites become exhausted the uptake rate depends on transportation from outside to inside the adsorbent particles (Udeozor and Ebuomwan 2014). However, the time of saturation totally equals with chlorpyrifos and cypermethrin. The observation obviously shows the specific time of saturation of 90 mins for chlorpyrifos and cypermethrin with adsorption capacity of 92.29% and 92.78% respectively.

Table 2. Contact time factor on adsorption capacity and percentage adsorption of cypermethrin and chlorpyrifos

| Adsorbate | Time | Co (mg/l) | Ce (mg/l) | X(mg/l) | Qe(mg/g) | % Adsorption |
|--------------|-------|-----------|-----------|---------|----------|--------------|
| Cypermethrin | 15 | 1.5 | 1.213 | 0.287 | 7.170 | 19.12 |
| | 30 | 1.5 | 0.674 | 0.827 | 20.663 | 55.1 |
| | 45 | 1.5 | 0.444 | 1.056 | 26.396 | 70.39 |
| | 60.0 | 1.5 | 0.278 | 1.222 | 30.544 | 81.45 |
| | 75 | 1.5 | 0.119 | 1.381 | 34.519 | 92.05 |
| | 90.0 | 1.5 | 0.116 | 1.384 | 34.609 | 92.29 |
| | 105.0 | 1.5 | 0.116 | 1.384 | 34.609 | 92.29 |
| Chlorpyrifos | 15 | 0.78 | 0.672 | 0.108 | 2.711 | 13.9 |
| | 30 | 0.78 | 0.651 | 0.129 | 3.231 | 16.57 |
| | 45 | 0.78 | 0.544 | 0.236 | 5.899 | 30.25 |
| | 60.0 | 0.78 | 0.145 | 0.635 | 15.877 | 81.42 |
| | 75 | 0.78 | 0.061 | 0.719 | 17.983 | 92.22 |
| | 90.0 | 0.78 | 0.057 | 0.723 | 18.067 | 92.78 |
| | 105.0 | 0.78 | 0.057 | 0.723 | 18.067 | 92.78 |

Adsorbent dosage 2g/50ml pH 6.3 temp. 30°C

Effect of pH on adsorption of chlorpyrifos and cypermethrin: The pH of the solution is an important controlling parameter in the adsorption process. The effect of pH on the adsorption uptake percent (%) of chlorpyrifos and cypermethrin is shown in table 3. From these data it is obvious that the percent adsorption gradually increases by increasing the pH till reaching maximum uptake at pH of 6.3. The adsorption percent of the each pesticide show similar trend. Meanwhile, the adsorption is low below pH 4.0 and increases rapidly at pH 5.6 getting to maximum at pH 6.3. At this pH of 6.3, 92.57% and 92.25% of chlorpyrifos and cypermethrin respectively were adsorbed. At higher pH the pesticides start degrading. The trend of the results is seen in the removal of carbofuran and chlorpyrifos from wastewater using walnut shell (Memon *et al* 2007)

Table 3. Effect of pH on adsorption capacity and percentage adsorption of cypermethrin and chlorpyrifos

| Adsorbate | pH | Co (mg/l) | Ce(mg/l) | X(mg/l) | Qe(mg/g) | % Adsorption |
|---------------|-----|-----------|----------|---------|----------|--------------|
| Cypermethrin | 2.2 | 1.5 | 1.360 | 0.140 | 3.499 | 9.33 |
| | 3.1 | 1.5 | 0.972 | 0.528 | 13.193 | 35.18 |
| | 4.1 | 1.5 | 0.529 | 0.971 | 24.285 | 64.76 |
| | 5.6 | 1.5 | 0.158 | 1.342 | 33.544 | 89.45 |
| | 6.3 | 1.5 | 0.116 | 1.384 | 34.594 | 92.25 |
| | 7.1 | 1.5 | 0.149 | 1.351 | 33.776 | 90.07 |
| | 7.5 | 1.5 | 0.245 | 1.255 | 31.365 | 83.64 |
| Chloropyrifos | 2.2 | 0.78 | 0.672 | 0.108 | 2.711 | 11.17 |
| | 3.1 | 0.78 | 0.651 | 0.129 | 3.231 | 46.87 |
| | 4.1 | 0.78 | 0.544 | 0.236 | 5.899 | 62.73 |
| | 5.6 | 0.78 | 0.145 | 0.635 | 15.877 | 88.52 |
| | 6.3 | 0.78 | 0.061 | 0.719 | 17.983 | 92.57 |
| | 7.1 | 0.78 | 0.057 | 0.723 | 18.067 | 89.76 |
| | 7.5 | 0.78 | 0.057 | 0.723 | 18.067 | 84.41 |

Adsorbent dosage 2g/50m temp. 30°C

Effect of initial concentration on adsorption: The effect of initial pesticide chloropyrifos and cypermethrin concentration in the range of 1.5 – 1.8 mg/l on adsorption was investigated and is shown in table 4. It is evident that the percentage pesticide removal increased with the increase in initial concentration of the pesticide. The initial pesticide concentration provides the necessary driving force to overcome the resistances to the mass transfer of pesticide between the aqueous phase and the solid phase. The driving force was observed to be greater in cypermethrin in which q_e (amount of adsorption per unit mass of adsorbent) of 87.5mg/g at initial concentration of 8.0 mg/l from 7.5mg/g at initial concentration of 1.5 mg/l. In chlorpyrifos q_e (amount of adsorption per unit mass of adsorbent) of 37.5mg/g at initial concentration of 7.0 mg/l from 5.0mg/g at initial concentration of 1.5 mg/l.

Isotherm Modelling: The adsorption isotherm data for the pesticide adsorption were as prepared in table 4. The graphical representations of these models are presented in figure 1 for Langmuir and figure 2 for Freundlich isotherm respectively. Each of the pesticide adsorbed per gram, (q_e) and respective equilibrium concentration (C_e) for each initial concentration of the pesticide was prepared. The plot of $1/q_e$ against the $1/C_e$ on shows straight lines as

displayed in figs. 1. This linear relationship is an indication that the adsorption process fit in and can be described by a Langmuir type isotherm. The fitting to Langmuir shows that the adsorption occurs mainly through the formation of a single monolayer of adsorbed molecules. Chloropyrifos adsorption fit better on Langmuir type isotherm

On the other hand, the plot of $\text{Log } q_e$ against the $\text{Log } C_e$ on shows straight lines as displayed in figs. 2 for cypermethrin and chlorpyrifos respectively this linear relationship is an indication that the adsorption process also fit in and can be described by a Freundlich isotherm. Cypermethrin adsorption was of course observed to fit better on Freundlich type isotherm

The isotherm equation is applied to describe the data in a quantitative way. (Okeola and Odebunmi, 2010). The isotherm parameters and correlation coefficient R^2 values are tabulated in table 6. When the value of correlation coefficient, R^2 is nearer to 1, the respective experimental data tend to fit better to the respective equation. The values of n (from Freundlich equation) greater than unity, suggesting favourable adsorption. The result of q_m (from Langmuir equation) shows an higher adsorption of cypermethrin under the same adsorption factor (Chang *et al* 2011)

Table 4: Effect of initial concentration on adsorption and Adsorption isotherm Data

| Adsorbate | Co (mg/l) | Ce(mg/l) | X(mg/l) | q _c (mg/g) | Log Ce | Log q _c | 1/q _c | 1/Ce |
|---------------|-----------|----------|---------|-----------------------|--------|--------------------|------------------|-------|
| Cypermethrin | 1.5 | 1.2 | 0.3 | 7.5 | 0.079 | 0.875 | 0.133 | 0.833 |
| | 2.5 | 1.9 | 0.6 | 15.0 | 0.279 | 1.176 | 0.067 | 0.526 |
| | 3.5 | 2.4 | 1.1 | 27.5 | 0.380 | 1.439 | 0.036 | 0.416 |
| | 4.0 | 2.6 | 1.4 | 35.0 | 0.415 | 1.544 | 0.028 | 0.384 |
| | 6.0 | 3.9 | 2.1 | 52.5 | 0.591 | 1.720 | 0.019 | 0.256 |
| | 8.0 | 4.5 | 3.5 | 87.5 | 0.653 | 1.942 | 0.011 | 0.222 |
| Chloropyrifos | 1.5 | 1.3 | 0.2 | 5.0 | 0.114 | 0.699 | 0.200 | 0.769 |
| | 2.0 | 1.7 | 0.3 | 7.5 | 0.230 | 0.875 | 0.133 | 0.588 |
| | 3.2 | 2.6 | 0.6 | 15.0 | 0.415 | 1.176 | 0.067 | 0.385 |
| | 4.0 | 3.0 | 1.0 | 25.0 | 0.477 | 1.398 | 0.040 | 0.333 |
| | 6.0 | 4.8 | 1.2 | 30.0 | 0.681 | 1.477 | 0.033 | 0.208 |
| | 7.0 | 5.5 | 1.5 | 37.5 | 0.740 | 1.574 | 0.027 | 0.181 |

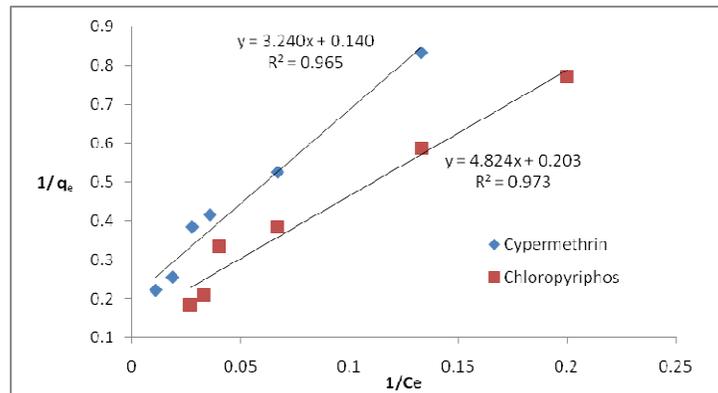


Fig 1: Langmuir adsorption of isotherm of cypermethrin and chloropyrifos adsorption

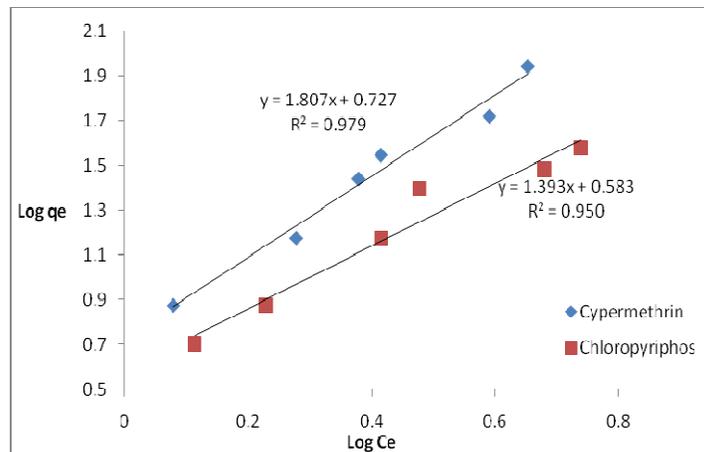


Fig 2: Freundlich adsorption of isotherm of cypermethrin and chloropyrifos adsorption

Table 5: Isotherm constants for cypermethrin and chloropyrifos adsorption

| Pesticide | Freundlich | | Langmuir | |
|---------------|----------------|-------|----------------|-------|
| cypermethrin | R ² | 0.979 | R ² | 0.973 |
| | K _f | 9.53 | K _L | 0.454 |
| | n | 5.33 | q _m | 7.14 |
| chloropyrifos | R ² | 0.950 | R ² | 0.965 |
| | K _f | 8.91 | K _L | 0.974 |
| | n | 3.83 | q _m | 4.93 |

Conclusion: In this study the feasibility of *curcas* shell for the adsorption of cypermethrin and application of the activated carbon from *jatropha* Chloropyrifos adsorption was established. The OKEOLA, FO; ODEBUNMI, EO; NWOSU, FO; ABU, TO; IDIAGBONYA, OS;³ AMOLOYE, MA; ONIFADE, FT; ABDULMUMMEEN, AG

adsorption depends on pH, contact time, mass of the sample and initial concentration of the pesticide. The adsorption process of cypermethrin and Chlorpyrifos fits better on Freundlich and Langmuir isotherms respectively.

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